



June 12, 2020

BP Products North America, Inc.  
Whiting Refinery  
2815 Indianapolis Blvd.  
Whiting, IN 46394

Attention: Mr. Joseph Schuler

Subject: Engineering Emission Test  
FCCU 500 Exhaust  
BP Products North America, Inc.: Whiting, Indiana  
Document No. M024AS-748176-RT-589

Dear Mr. Schuler:

Montrose Air Quality Services, LLC (Montrose) was contracted by BP Products North America, Inc. (BP) to conduct a particulate matter (PM) engineering emission test on the Fluidized Catalytic Cracking Unit (FCCU) 500 stack at their refinery located in Whiting, Indiana.

Testing was conducted on May 27, 2020 during an alternate ESP operating scenario to determine the concentrations and emission rates of total PM and PM under 10 microns (PM<sub>10</sub>), including condensable PM (CPM).

Testing was conducted generally pursuant to the following procedures:

- Code of Federal Regulations, Title 40, Part 60 (40 CFR 60), Appendix A, USEPA Methods 1-4
- 40 CFR 51, Appendix M, USEPA Methods 201A and 202

Two engineering test runs were conducted with samples collected simultaneously in two Method 201A/202 sampling trains (four samples total). The first test repetition was 120 minutes in duration. The second test repetition was shortened to 90 minutes due to adverse weather that was approaching the facility.

Train A was sampled from the northwest sample port, and Train B was sampled from the southwest sample port. A full USEPA Method 1 traverse was not conducted during sampling. During each test run, the probe was traversed at the Method 1 test points across the single port in which it was inserted.

Mr. Joseph Schuler of BP coordinated the test and monitored process conditions. Testing was conducted by Mr. Steve Flaherty, Mr. Vannak Khy, Mr. Matthew Krueger, and Mr. Urbano Leos of Montrose. Mr. Steve Flaherty was the onsite field test supervisor and qualified source testing individual for the test.

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BP Products North America, Inc.: Whiting, Indiana  
May 2020 FCCU 500 Engineering Emission Test

The test results are presented in Tables 1 and 2. The calculation summaries, field data, and laboratory data are included in the attachments.

If you have any questions, please do not hesitate to contact me at (847) 487-1580 Ext. 12417 or [sflaherty@montrose-env.com](mailto:sflaherty@montrose-env.com).

Respectfully submitted,



Steve Flaherty  
Midwest District Manager  
**Montrose Air Quality Services, LLC**

SF:do  
Attachments

**TABLE 1**  
**FCCU 500 STACK PM<sub>10</sub> AND TOTAL PM ENGINEERING TEST RESULTS (RUN 1)**

TEST RUN NO. :	1-A	1-B	
TEST DATE :	5/27/2020	5/27/2020	
TEST TIME :	08:50-10:50	08:50-10:52	Average
<b>Stack Gas Parameters</b>			
Temperature, °F	510.9	510.0	510.5
Velocity, av. ft/sec	82.3	83.5	82.9
Volumetric flow, acfm	314,163	318,572	316,367
Volumetric flow, scfm	166,832	169,352	168,092
Volumetric flow, scfh	10,009,911	10,161,093	10,085,502
Volumetric flow, dscfm	133,017	135,060	134,038
Volumetric flow, dscfh	7,981,007	8,103,588	8,042,297
Mass flow, Mlb/hr db	644.4	654.3	649.4
Moisture, av. % vol.	20.3	20.2	20.3
Molecular weight, lb/lb-mole db	31.1	31.1	31.1
Carbon dioxide, av. % vol. db	19.0	19.0	19.0
Oxygen, av. % vol. db	1.7	1.7	1.7
<b>Particulate Sample</b>			
Time, min.	120.33	122.80	121.57
Volume, dscf	36.124	39.247	37.685
> PM <sub>10</sub> , mg	34.75	36.45	35.60
Filterable PM <sub>10</sub> , mg	127.2	129.6	128.4
Condensable PM <sub>10</sub> , mg	8.40	10.85	9.63
Total PM <sub>10</sub> , mg	135.6	140.5	138.0
Isokinetic ratio, %	97.9	102.7	100.3
D <sub>50</sub> cutpoint, µm	10.57	10.12	10.35
<b>Filterable PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0543	0.0510	0.0526
x 10 <sup>-6</sup> lb/dscf	7.764	7.281	7.523
mg/dscm	124.351	116.617	120.484
Emission rate			
lb/hr	61.966	59.005	60.486
lb/1,000 lb coke burn	1.722	1.639	1.680
<b>Condensable PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0036	0.0043	0.0039
x 10 <sup>-6</sup> lb/dscf	0.513	0.610	0.561
mg/dscm	8.212	9.763	8.987
Emission rate			
lb/hr	4.092	4.940	4.516
lb/1,000 lb coke burn	0.114	0.137	0.125
<b>Total PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0579	0.0552	0.0566
x 10 <sup>-6</sup> lb/dscf	8.277	7.891	8.084
mg/dscm	132.563	126.380	129.471
Emission rate			
lb/hr	66.058	63.945	65.002
lb/1,000 lb coke burn	1.835	1.777	1.806

**TABLE 1 (CONTINUED)**  
**FCCU 500 STACK PM<sub>10</sub> AND TOTAL PM ENGINEERING TEST RESULTS (RUN 1)**

TEST RUN NO. :	1-A	1-B	
TEST DATE :	5/27/2020	5/27/2020	
TEST TIME :	08:50-10:50	08:50-10:50	Average
<b>Filterable &gt; PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0148	0.0143	0.0146
x 10 <sup>-6</sup> lb/dscf	2.121	2.048	2.085
mg/dscm	33.972	32.799	33.385
Emission rate			
lb/hr	16.929	16.595	16.762
lb/1,000 lb coke burn	0.470	0.461	0.466
<b>Total PM (PM<sub>10</sub> + &gt; PM<sub>10</sub>)</b>			
Concentration			
grains/dscf	0.0728	0.0695	0.0711
x 10 <sup>-6</sup> lb/dscf	10.398	9.939	10.169
mg/dscm	166.534	159.179	162.857
Emission rate			
lb/hr	82.987	80.540	81.764
lb/1,000 lb coke burn	2.306	2.238	2.272

**TABLE 2**  
**FCCU 500 STACK PM<sub>10</sub> AND TOTAL PM ENGINEERING TEST RESULTS (RUN 2)**

TEST RUN NO. :	2-A	2-B	
TEST DATE :	5/27/2020	5/27/2020	
TEST TIME :	12:17-13:47	12:17-13:50	Average
<b>Stack Gas Parameters</b>			
Temperature, °F	513.6	510.0	511.8
Velocity, av. ft/sec	82.6	84.9	83.7
Volumetric flow, acfm	315,193	324,118	319,656
Volumetric flow, scfm	166,915	172,300	169,607
Volumetric flow, scfh	10,014,892	10,337,994	10,176,443
Volumetric flow, dscfm	134,379	137,867	136,123
Volumetric flow, dscfh	8,062,711	8,272,031	8,167,371
Mass flow, Mlb/hr db	651.0	667.9	659.5
Moisture, av. % vol.	19.5	20.0	19.7
Molecular weight, lb/lb-mole db	31.1	31.1	31.1
Carbon dioxide, av. % vol. db	19.0	19.0	19.0
Oxygen, av. % vol. db	1.7	1.7	1.7
<b>Particulate Sample</b>			
Time, min.	90.70	93.30	92.00
Volume, dscf	27.664	29.043	28.353
> PM <sub>10</sub> , mg	22.30	28.60	25.45
Filterable PM <sub>10</sub> , mg	89.0	83.6	86.3
Condensable PM <sub>10</sub> , mg	5.50	6.30	5.90
Total PM <sub>10</sub> , mg	94.5	89.9	92.2
Isokinetic ratio, %	98.5	98.0	98.3
D <sub>50</sub> cutpoint, µm	10.54	10.34	10.44
<b>Filterable PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0496	0.0444	0.0470
x 10 <sup>-6</sup> lb/dscf	7.090	6.343	6.717
mg/dscm	113.552	101.594	107.573
Emission rate			
lb/hr	57.164	52.472	54.818
lb/1,000 lb coke burn	1.589	1.458	1.523
<b>Condensable PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0031	0.0033	0.0032
x 10 <sup>-6</sup> lb/dscf	0.438	0.478	0.458
mg/dscm	7.021	7.661	7.341
Emission rate			
lb/hr	3.535	3.957	3.746
lb/1,000 lb coke burn	0.098	0.110	0.104
<b>Total PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0527	0.0477	0.0502
x 10 <sup>-6</sup> lb/dscf	7.528	6.822	7.175
mg/dscm	120.573	109.255	114.914
Emission rate			
lb/hr	60.699	56.429	58.564
lb/1,000 lb coke burn	1.687	1.568	1.628

**TABLE 2 (CONTINUED)**  
**FCCU 500 STACK PM<sub>10</sub> AND TOTAL PM ENGINEERING TEST RESULTS (RUN 2)**

TEST RUN NO. :	2-A	2-B	
TEST DATE :	5/27/2020	5/27/2020	
TEST TIME :	12:17-13:47	12:17-13:50	Average
<b>Filterable &gt; PM<sub>10</sub></b>			
Concentration			
grains/dscf	0.0124	0.0152	0.0138
x 10 <sup>-6</sup> lb/dscf	1.777	2.171	1.974
mg/dscm	28.468	34.777	31.622
Emission rate			
lb/hr	14.331	17.962	16.147
lb/1,000 lb coke burn	0.398	0.499	0.449
<b>Total PM (PM<sub>10</sub> + &gt; PM<sub>10</sub>)</b>			
Concentration			
grains/dscf	0.0651	0.0629	0.0640
x 10 <sup>-6</sup> lb/dscf	9.306	8.993	9.150
mg/dscm	149.041	144.032	146.537
Emission rate			
lb/hr	75.030	74.391	74.711
lb/1,000 lb coke burn	2.085	2.067	2.076

## **ATTACHMENT A CALCULATION SUMMARIES**

**USEPA Method 2**  
**Volumetric Flow Rate Sample Calculations (Circular Ducts)**

**Client:** BP  
**Location:** Whiting, IN  
**Source:** FCCU 500  
**Date:** 5/27/2020  
**Run #:** 1-A

**Data Input**

<b>Carbon Dioxide (CO<sub>2</sub>):</b>	19.0 %
<b>Oxygen (O<sub>2</sub>):</b>	1.7 %
<b>Nitrogen (N<sub>2</sub>):</b>	79.3 %
<b>Fractional Moisture Content (B<sub>wo</sub>)</b>	0.2027
<b>Stack Temperature (T<sub>s</sub>):</b>	510.9 °F
<b>Pitot Coefficient (C<sub>p</sub>):</b>	0.84 dimensionless
<b>Average square root of ΔP</b>	1.0605 inches H <sub>2</sub> O
<b>Barometric Pressure (P<sub>bar</sub>):</b>	29.29 inches Hg
<b>Static Pressure (S<sub>t</sub>)</b>	-1.00 inches H <sub>2</sub> O
<b>Stack diameter:</b>	108.00 inches H <sub>2</sub> O
<b>Stack area (A<sub>s</sub>):</b>	63.6172 ft <sup>2</sup>

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Dry molecular weight of stack gas:**

$$M_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2) = 31.108 \text{ lb/lb-mole}$$

**Molecular weight of stack gas, wet basis:**

$$M_s = (M_d \times (1 - B_{ws})) + (18 \times B_{ws}) = 28.451 \text{ lb/lb-mole}$$

**Absolute stack gas pressure:**

$$P_s = P_{bar} + \left( \frac{S_t}{13.6} \right) = 29.216 \text{ inches H}_2\text{O}$$

**Stack gas velocity:**

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{(T_s + 460)}{(P_s \times M_s)}} = 82.305 \text{ feet/second}$$

**Stack gas volumetric flow rate:**

$$Q_a = A_s \times V_s \times 60 = 314,163 \text{ acfm}$$

**Stack gas volumetric flow rate, wet basis:**

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] = 166,832 \text{ scfm}$$

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] \times 60 = 10,009,911 \text{ scfh}$$

**Stack gas volumetric flow rate, dry basis:**

$$Q_{std} = Q_{sw} \times (1 - B_{wo}) = 133,017 \text{ dscfm}$$

$$Q_{std} = Q_{sw} \times (1 - B_{wo}) \times 60 = 7,981,007 \text{ dscfh}$$



# USEPA Method 4 Moisture Determination Sample Calculations

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 1-A

## Data Input:

Volume metered ( $V_m$ ):	39.405 ft <sup>3</sup>
Meter calibration coefficient ( $Y_d$ ):	0.995 dimensionless
Barometric pressure ( $P_{bar}$ ):	29.29 inches Hg
Meter sample rate ( $\Delta H$ ):	0.35 inches H <sub>2</sub> O
Meter inlet/outlet temperature ( $T_m$ ):	101.5 °F
Volume of moisture collected ( $V_{lc}$ ):	195.1 milliliters
Stack Temperature ( $T_s$ ):	510.9 °F
Static Pressure ( $St$ ):	-1.0 inches H <sub>2</sub> O

## Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):

### Volume of sample, dry basis:

$$V_{m_{std}} = V_m \times Y_d \times \left( \frac{528.0^\circ R}{29.92 \text{ "Hg}} \right) \times \left( \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m + 460} \right) = 36.124 \text{ dscf}$$

### Volume of water vapor in sample:

$$V_{w_{std}} = \frac{0.04707 \text{ ft}^3}{\text{ml}} \times V_{lc} = 9.183 \text{ scf}$$

### Fractional moisture content of stack gas:

$$B_{wo} = \frac{V_{w_{std}}}{(V_{m_{std}} + V_{w_{std}})} = 0.2027 B_{wo}$$

### Percent Moisture:

$$\% \text{moisture} = B_{wo} \times 100 = 20.27 \%$$

### Fractional moisture content of stack gas at saturated conditions:

$$T_{s(K)} = ((T_s - 32) \times 0.5556) + 273 = 539.1 \text{ °Kelvin}$$

$$P_{s(\text{mmHg})} = \left( P_{bar} + \frac{St}{13.6} \right) \times 25.401 = 744.00 \text{ mm Hg}$$

$$B_{wos} = \frac{\sqrt{10^{\left( A - \left( \frac{B}{(T_{s(K)} - C) \right) \right)}}}{P_{s(\text{mmHg})}} \quad \begin{array}{l} \text{where:} \\ A = 8.361 \\ B = 1893.5 \\ C = 27.65 \end{array} = 1.00$$

### Percent moisture at saturated conditions:

$$\% \text{moisture}_{\text{saturated}} = B_{wos} \times 100 = 100.00 \%$$

### Percent moisture used for emissions calculations:

$$= 20.27 \%$$

**USEPA Method 201A PM<sub>10</sub> Emissions  
D<sub>50</sub> Cutpoint Calculation Summary**

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 1-A

**Data Input**

Stack temperature (T <sub>s</sub> ):	510.9 °F
Fractional Moisture content (B <sub>ws</sub> ):	0.2027
Oxygen (O <sub>2</sub> ):	1.7 %
Stack pressure (P <sub>s</sub> ):	29.22 Inches Hg Abs.
Volume metered (V <sub>mstd</sub> ):	36.124 dscf
Volume of water vapor (V <sub>wstd</sub> ):	9.183 scf
Molecular weight of gas, wet basis (M <sub>s</sub> ):	28.451 lb/lb-mole
Test length (t):	120.33 minutes
D <sub>p</sub> :	10.0 microns

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Stack gas viscosity:**

$$\mu = -150.3162 + \left(13.4622 \times \sqrt{(T_s + 460)}\right) + \left(3.86153 \times 10^{-6} \times (T_s + 460)^{-2}\right) + \left(0.591123 \times (\%O_{2, wet})\right) - (91.9723 \times B_{ws}) + \left(1.51761 \times 10^{-5} \times B_{ws} \times (T_s + 460)^2\right)$$

= 258.31 micropoise

**Sample flow rate @ standard conditions:**

$$Q_{sSt} = \frac{V_{mstd}}{t}$$

= 0.300 dscfm

**Sample flow rate through PM<sub>10</sub> cyclone:**

$$Q_s = \frac{29.92}{528} \times Q_{sSt} \times \left(\frac{1}{(1 - B_{ws})}\right) \times \left(\frac{[T_s + 460]}{P_s}\right)$$

= 0.709 cfm

**Calculated Reynolds Number**

$$N_{re} = 8.64 \times 10^5 \times \left(\frac{P_s \times M_s}{(T_s + 460)}\right) \times \left(\frac{Q_s}{\mu}\right)$$

= 2030

**Cunningham Correction Factor**

$$C = 1 + 0.0057193 \times \left(\frac{\mu}{P_s \times D_p}\right) \times \left(\left(\frac{[T_s + 460]}{M_s}\right)^{0.50}\right)$$

= 1.0295

**D<sub>50</sub> cutpoint (for Cyclone I):**

$$D_{50} = \left(0.15625 \times \left(\frac{[T_s + 460]}{(M_s \times P_s)}\right)^{0.2091}\right) \times \left(\frac{\mu}{Q_s}\right)^{0.7091}$$

= 10.575 μm

**USEPA Method 202  
Condensible Particulate Calculation Summary**

COMPANY: BP  
LOCATION: Whiting, IN  
SOURCE: FCCU 500  
TEST DATE: 5/27/20  
RUN NUMBER: 1-A

**Data Input:**

$V_m$ :	39.405	ft <sup>3</sup>	$Q_s$ :	133,017	dscfm
$\gamma$ FACTOR:	0.995		$T_s$ :	510.9	°F
$P_{bar}$ :	29.29	in.Hg	Runtime:	120.33	minutes
$\Delta H$ :	0.35	in.H <sub>2</sub> O	$V_s$ :	82.305	ft/sec
$T_m$ :	101.5	°F	$P_s$ :	29.22	in.Hg
$V_{lc}$ :	195.1	mL	Noz. diam:	0.164	inches
$N$ :	0.0000		$m_{lb}$ :	0.00	mg
$V_t$ :	0.00	mL	$m_{ob}$ :	0.00	mg
$m_r$ :	6.80	mg			
$m_o$ :	1.60	mg			

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Volume of sample at standard conditions:**

$$V_{mstd} = \left( \frac{528}{29.92} \right) \times V_m \times \gamma \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right] = 36.124 \text{ dscf}$$

**Mass of ammonia correction:**

$$m_c = 17.03 \times V_T \times N = 0.00 \text{ mg}$$

**Mass of the field blank:**

$$m_{fb} = m_{lb} + m_{ob} = 0.00 \text{ mg}$$

**Mass of inorganic condensible PM:**

$$m_i = m_r - m_c = 6.80 \text{ mg}$$

**Total mass of condensible PM:**

$$m_{cpm} = m_i + m_o - m_{fb} = 8.40 \text{ mg}$$

**USEPA Method 201A PM<sub>10</sub> Emissions  
Particulate Calculation Summary**

**Client:** BP  
**Location:** Whiting, IN  
**Source:** FCCU 500  
**Date:** 5/27/2020  
**Run #:** 1-A

**Data Input**

Barometric pressure (P <sub>bar</sub> ):	29.29 inches Hg	<b>Particulate Weight:</b>	
Stack pressure (P <sub>s</sub> ):	29.22 inches Hg Abs.	<PM10 (Filterable)	113.55 milligrams
Test length (t):	120.33 minutes	>PM10 (Cyclone Catch)	34.75 milligrams
Sample nozzle diameter (D <sub>n</sub> ):	0.1640 inches		
Sample nozzle area (A <sub>n</sub> ):	0.000147 ft <sup>2</sup>	<PM10 (Probe Wash)	13.65 milligrams
Stack temperature (T <sub>s</sub> ):	510.9 °F	Total PM <sub>10</sub> front half:	127.20 milligrams
Volume metered (V <sub>mstd</sub> ):	36.124 ft <sup>3</sup>		
Stack gas velocity (V <sub>s</sub> ):	82.305 feet/second	Total PM front half	161.95 milligrams
Stack gas volumetric flow (Q <sub>std</sub> ):	7,981,007 dscf/hour	Total corrected PM <sub>10</sub> back half:	8.40 milligrams
Fractional moisture content (B <sub>wo</sub> ):	0.2027		
Coke Burn Rate (R <sub>c</sub> ):	35,993 lb/hr		
		Total PM <sub>10</sub> weight (M <sub>n</sub> ):	135.60 milligrams
		Total PM weight (M <sub>n</sub> ):	170.35 milligrams (>PM <sub>10</sub> + PM <sub>10</sub> )

**Sample calculations @ standard conditions (29.92 inches Hg, 88.0 °F):**

**Percent Isokinetic:**

$$\% \text{isokinetic} = \frac{0.0945 \times V_{mstd} \times (T_s + 460)}{P_s \times V_s \times t \times A_n \times (1 - B_{wo})} = 97.9 \% \text{ isokinetic}$$

**PM<sub>10</sub> and Total Particulate emission rate (lb/dscf):**

$$C_s = \frac{\left( \frac{0.01543 \text{ grains}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.0728 \text{ total PM gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0148 \text{ >PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.0543 \text{ filterable PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0036 \text{ condensible PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0579 \text{ PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 166.634 \text{ total PM mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 33.972 \text{ >PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 124.351 \text{ filterable PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 8.212 \text{ condensible PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 132.563 \text{ PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 10.398 \times 10^{-6} \text{ total PM lb/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 2.121 \times 10^{-6} \text{ >PM}_{10} \text{ lb/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 7.764 \times 10^{-6} \text{ filterable PM}_{10} \text{ lb/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.513 \times 10^{-6} \text{ condensible PM}_{10} \text{ lb/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 8.277 \times 10^{-6} \text{ PM}_{10} \text{ lb/dscf}$$

**PM<sub>10</sub> and Total Particulate emission rate (lb/hr):**

$$E_p = C_s \times Q_{std} = 82.987 \text{ total PM lb/hr}$$

$$E_p = C_s \times Q_{std} = 16.929 \text{ >PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 61.968 \text{ filterable PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 4.092 \text{ condensible PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 66.058 \text{ PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 2.306 \text{ total PM lb/1000lb coke burn}$$

$$E_p = C_s \times Q_{std} = 0.470 \text{ >PM}_{10} \text{ lb/1000lb coke burn}$$

$$E_p = C_s \times Q_{std} = 1.722 \text{ filterable PM}_{10} \text{ lb/1000lb coke burn}$$

$$E_p = C_s \times Q_{std} = 0.114 \text{ condensible PM}_{10} \text{ lb/1000 coke burn}$$

$$E_p = C_s \times Q_{std} = 1.836 \text{ PM}_{10} \text{ lb/1000 coke burn}$$

**USEPA Method 2**  
**Volumetric Flow Rate Sample Calculations (Circular Ducts)**

**Client:** BP  
**Location:** Whiting, IN  
**Source:** FCCU 500  
**Date:** 5/27/2020  
**Run #:** 1-B

**Data Input**

Carbon Dioxide (CO <sub>2</sub> ):	19.0 %
Oxygen (O <sub>2</sub> ):	1.7 %
Nitrogen (N <sub>2</sub> ):	79.3 %
Fractional Moisture Content (B <sub>w0</sub> )	0.2025
Stack Temperature (T <sub>s</sub> ):	510.0 °F
Pitot Coefficient (C <sub>p</sub> ):	0.84 dimensionless
Average square root of ΔP	1.0760 inches H <sub>2</sub> O
Barometric Pressure (P <sub>bar</sub> ):	29.29 inches Hg
Static Pressure (S <sub>i</sub> )	-0.95 inches H <sub>2</sub> O
Stack diameter:	108.00 inches H <sub>2</sub> O
Stack area (A <sub>s</sub> ):	63.6172 ft <sup>2</sup>

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Dry molecular weight of stack gas:**

$$M_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2) = 31.108 \text{ lb/lb-mole}$$

**Molecular weight of stack gas, wet basis:**

$$M_s = (M_d \times (1 - B_{ws})) + (18 \times B_{ws}) = 28.454 \text{ lb/lb-mole}$$

**Absolute stack gas pressure:**

$$P_s = P_{bar} + \left( \frac{S_i}{13.6} \right) = 29.220 \text{ inches H}_2\text{O}$$

**Stack gas velocity:**

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{(T_s + 460)}{(P_s \times M_s)}} = 83.461 \text{ feet/second}$$

**Stack gas volumetric flow rate:**

$$Q_a = A_s \times V_s \times 60 = 318,572 \text{ acfm}$$

**Stack gas volumetric flow rate, wet basis:**

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] = 169,352 \text{ scfm}$$

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] \times 60 = 10,161,093 \text{ scfh}$$

**Stack gas volumetric flow rate, dry basis:**

$$Q_{std} = Q_{sw} \times (1 - B_{w0}) = 135,060 \text{ dscfm}$$

$$Q_{std} = Q_{sw} \times (1 - B_{w0}) \times 60 = 8,103,588 \text{ dscfh}$$

**USEPA Method 4**  
**Moisture Determination Sample Calculations**

**Client:** BP  
**Location:** Whiting, IN  
**Source:** FCCU 500  
**Date:** 5/27/2020  
**Run #:** 1-B

**Data Input:**

<b>Volume metered (<math>V_m</math>):</b>	42.506 ft <sup>3</sup>
<b>Meter calibration coefficient (<math>Y_d</math>):</b>	1.009 dimensionless
<b>Barometric pressure (<math>P_{bar}</math>):</b>	29.29 inches Hg
<b>Meter sample rate (<math>\Delta H</math>):</b>	0.32 inches H <sub>2</sub> O
<b>Meter inlet/outlet temperature (<math>T_m</math>):</b>	105.3 °F
<b>Volume of moisture collected (<math>V_{lc}</math>):</b>	211.7 milliliters
<b>Stack Temperature (<math>T_s</math>):</b>	510.0 °F
<b>Static Pressure (<math>S_t</math>):</b>	-1.0 inches H <sub>2</sub> O

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Volume of sample, dry basis:**

$$V_{m_{std}} = V_m \times Y_d \times \left( \frac{528.0^\circ R}{29.92'' \text{ Hg}} \right) \times \left( \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m + 460} \right) = 39.247 \text{ dscf}$$

**Volume of water vapor in sample:**

$$V_{w_{std}} = \frac{0.04707 \text{ ft}^3}{\text{ml}} \times V_{lc} = 9.965 \text{ scf}$$

**Fractional moisture content of stack gas:**

$$B_{wo} = \frac{V_{w_{std}}}{(V_{m_{std}} + V_{w_{std}})} = 0.2025 B_{wo}$$

**Percent Moisture:**

$$\% \text{moisture} = B_{wo} \times 100 = 20.25 \%$$

**Fractional moisture content of stack gas at saturated conditions:**

$$T_{s(K)} = ((T_s - 32) * 0.5556) + 273 = 538.6 \text{ °Kelvin}$$

$$P_{s(\text{mmHg})} = \left( P_{bar} + \frac{S_t}{13.6} \right) \times 25.401 = 744.00 \text{ mm Hg}$$

$$B_{wos} = \frac{\sqrt{10 \left( A - \left( \frac{B}{(T_s(K) - C)} \right) \right)}}{P_{s(\text{mmHg})}} \quad \begin{array}{l} \text{where:} \\ A = 8.361 \\ B = 1893.5 \\ C = 27.65 \end{array} = 1.00$$

**Percent moisture at saturated conditions:**

$$\% \text{moisture}_{\text{saturated}} = B_{wos} \times 100 = 100.00 \%$$

**Percent moisture used for emissions calculations:**

$$= 20.25 \%$$

**USEPA Method 201A PM<sub>10</sub> Emissions  
D<sub>50</sub> Cutpoint Calculation Summary**

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 1-B

**Data Input**

Stack temperature (T <sub>s</sub> ):	510.0 °F
Fractional Moisture content (B <sub>ws</sub> ):	0.2025
Oxygen (O <sub>2</sub> ):	1.7 %
Stack pressure (P <sub>s</sub> ):	29.22 Inches Hg Abs.
Volume metered (V <sub>mstd</sub> ):	39.247 dscf
Volume of water vapor (V <sub>wstd</sub> ):	9.965 scf
Molecular weight of gas, wet basis (M <sub>s</sub> ):	28.454 lb/lb-mole
Test length (t):	122.80 minutes
D <sub>p</sub> :	10.0 microns

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Stack gas viscosity:**

$$\mu = -150.3162 + \left(13.4622 \times \sqrt{(T_s + 460)}\right) + \left(3.86153 \times 10^{-6} \times (T_s + 460)^{-2}\right) + \left(0.591123 \times (\%O_{2, \text{wet}})\right) - (91.9723 \times B_{ws}) + \left(1.51761 \times 10^{-5} \times B_{ws} \times (T_s + 460)^2\right)$$

= 258.1 micropoise

**Sample flow rate @ standard conditions:**

$$Q_{sSt} = \frac{V_{mstd}}{t}$$

= 0.320 dscfm

**Sample flow rate through PM<sub>10</sub> cyclone:**

$$Q_s = \frac{29.92}{528} \times Q_{sSt} \times \left(\frac{1}{(1 - B_{ws})}\right) \times \left(\frac{[T_s + 460]}{P_s}\right)$$

= 0.754 cfm

**Calculated Reynolds Number**

$$N_{re} = 8.64 \times 10^5 \times \left(\frac{P_s \times M_s}{(T_s + 460)}\right) \times \left(\frac{Q_s}{\mu}\right)$$

= 2163

**Cunningham Correction Factor**

$$C = 1 + 0.0057193 \times \left(\frac{\mu}{P_s \times D_p}\right) \times \left(\left(\frac{[T_s + 460]}{M_s}\right)^{0.50}\right)$$

= 1.030

**D<sub>50</sub> cutpoint (for Cyclone I):**

$$D_{50} = \left(0.15625 \times \left(\frac{[T_s + 460]}{(M_s \times P_s)}\right)^{0.2091}\right) \times \left(\frac{\mu}{Q_s}\right)^{7.091}$$

= 10.118 μm

**USEPA Method 202**  
**Condensible Particulate Calculation Summary**

COMPANY: BP  
 LOCATION: Whiting, IN  
 SOURCE: FCCU 500  
 TEST DATE: 5/27/20  
 RUN NUMBER: 1-B

**Data Input:**

V <sub>m</sub> :	42.506	ft <sup>3</sup>	Q <sub>s</sub> :	135,060	dscfm
γ FACTOR:	1.009		T <sub>s</sub> :	510.0	°F
P <sub>bar</sub> :	29.29	in.Hg	Runtime:	122.80	minutes
ΔH:	0.32	in.H <sub>2</sub> O	V <sub>s</sub> :	83.461	ft/sec
T <sub>m</sub> :	105.3	°F	P <sub>s</sub> :	29.22	in.Hg
V <sub>ic</sub> :	211.7	mL	Noz. diam:	0.164	inches
N:	0.0000		m <sub>ib</sub> :	0.00	mg
V <sub>t</sub> :	0.23	mL	m <sub>ob</sub> :	0.00	mg
m <sub>r</sub> :	9.35	mg			
m <sub>o</sub> :	1.50	mg			

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Volume of sample at standard conditions:**

$$V_{mstd} = \left( \frac{528}{29.92} \right) \times V_m \times \gamma \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right] = 39.247 \text{ dscf}$$

**Mass of ammonia correction:**

$$m_c = 17.03 \times V_T \times N = 0.00 \text{ mg}$$

**Mass of the field blank:**

$$m_{fb} = m_{ib} + m_{ob} = 0.00 \text{ mg}$$

**Mass of inorganic condensible PM:**

$$m_i = m_r - m_c = 9.35 \text{ mg}$$

**Total mass of condensible PM:**

$$m_{cpm} = m_i + m_o - m_{fb} = 10.85 \text{ mg}$$



**USEPA Method 201A PM10 Emissions  
Particulate Calculation Summary**

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 1-B

**Data Input**

Barometric pressure (P <sub>bar</sub> ):	29.29 inches Hg	Particulate Weight:	
Stack pressure (P <sub>s</sub> ):	29.22 Inches Hg Abs.	<PM10 (Filterable)	118.50 milligrams
Test length (t):	122.80 minutes	>PM10 (Cyclone Catch)	36.45 milligrams
Sample nozzle diameter (D <sub>n</sub> ):	0.1640 inches		
Sample nozzle area (A <sub>n</sub> ):	0.000147 ft <sup>2</sup>	<PM10 (Probe Wash)	11.10 milligrams
Stack temperature (T <sub>s</sub> ):	510.0 °F	Total PM <sub>10</sub> front half:	129.60 milligrams
Volume metered (V <sub>mstd</sub> ):	39.247 ft <sup>3</sup>		
Stack gas velocity (V <sub>s</sub> ):	83.461 feet/second	Total PM front half	166.05 milligrams
Stack gas volumetric flow (Q <sub>std</sub> ):	8,103,588 dscf/hour	Total corrected PM <sub>10</sub> back half:	10.85 milligrams
Fractional Moisture content (B <sub>we</sub> ):	0.2025		
Coke Burn Rate (R <sub>c</sub> ):	35,993 lb/hr	Total PM <sub>10</sub> weight (M <sub>n</sub> ):	140.45 milligrams
		Total PM weight (M <sub>n</sub> ):	176.90 milligrams (>PM <sub>10</sub> + PM <sub>10</sub> )

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Percent Isokinetic:**

$$\% \text{isokinetic} = \frac{0.0945 \times V_{mstd} \times (T_s + 460)}{P_s \times V_s \times 0 \times A_n \times (1 - B_{we})} = 102.7 \% \text{ isokinetic}$$

**PM<sub>10</sub> and Total Particulate emission rate (lb/dscf):**

$$C_s = \frac{\left( \frac{0.01543 \text{ grains}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.0695 \text{ total PM gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0143 > \text{PM}_{10} \text{ gr/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.0510 \text{ filterable PM}_{10} \text{ gr/dscf}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0043 \text{ condensible PM}_{10} \text{ gr/dscf}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0652 \text{ PM}_{10} \text{ gr/dscf}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 159.179 \text{ total PM mg/dscm}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 32.799 > \text{PM}_{10} \text{ mg/dscm}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 116.617 \text{ filterable PM}_{10} \text{ mg/dscm}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 9.763 \text{ condensible PM}_{10} \text{ mg/dscm}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 126.380 \text{ PM}_{10} \text{ mg/dscm}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 9.939 \times 10^{-6} \text{ total PM lb/dscf}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 2.048 \times 10^{-6} > \text{PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 7.281 \times 10^{-6} \text{ filterable PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.610 \times 10^{-6} \text{ condensible PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 7.891 \times 10^{-6} \text{ PM}_{10} \text{ lb/dscf}$$

**PM<sub>10</sub> and Total Particulate emission rate (lb/hr):**

$$E_p = C_s \times Q_{std} = 80.540 \text{ total PM lb/hr}$$

$$E_p = C_s \times Q_{std} = 16.595 > \text{PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 59.005 \text{ filterable PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 4.940 \text{ condensible PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 63.945 \text{ PM}_{10} \text{ lb/hr}$$

$$\text{pmr}_{\text{lb}/1000\text{lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 2.238 \text{ total PM lb/1000lb coke burn}$$

$$\text{pmr}_{\text{lb}/1000\text{lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 0.461 > \text{PM}_{10} \text{ lb/1000lb coke burn}$$

$$\text{pmr}_{\text{lb}/1000\text{lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 1.639 \text{ filterable PM}_{10} \text{ lb/1000lb coke burn}$$

$$\text{pmr}_{\text{lb}/1000\text{lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 0.137 \text{ condensible PM}_{10} \text{ lb/1000 coke burn}$$

$$\text{pmr}_{\text{lb}/1000\text{lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 1.777 \text{ PM}_{10} \text{ lb/1000 coke burn}$$

**USEPA Method 2**  
**Volumetric Flow Rate Sample Calculations (Circular Ducts)**

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 2-A

**Data Input**

Carbon Dioxide (CO <sub>2</sub> ):	19.0 %
Oxygen (O <sub>2</sub> ):	1.7 %
Nitrogen (N <sub>2</sub> ):	79.3 %
Fractional Moisture Content (B <sub>wo</sub> )	0.1949
Stack Temperature (T <sub>s</sub> ):	513.6 °F
Pitot Coefficient (C <sub>p</sub> ):	0.84 dimensionless
Average square root of ΔP	1.0644 inches H <sub>2</sub> O
Barometric Pressure (P <sub>bar</sub> ):	29.29 inches Hg
Static Pressure (S <sub>i</sub> )	-1.00 inches H <sub>2</sub> O
Stack diameter:	108.00 inches H <sub>2</sub> O
Stack area (A <sub>s</sub> ):	63.6172 ft <sup>2</sup>

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Dry molecular weight of stack gas:**

$$M_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2) = 31.108 \text{ lb/lb-mole}$$

**Molecular weight of stack gas, wet basis:**

$$M_s = (M_d \times (1 - B_{ws})) + (18 \times B_{ws}) = 28.553 \text{ lb/lb-mole}$$

**Absolute stack gas pressure:**

$$P_s = P_{bar} + \left( \frac{S_i}{13.6} \right) = 29.216 \text{ inches H}_2\text{O}$$

**Stack gas velocity:**

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{(T_s + 460)}{(P_s \times M_s)}} = 82.575 \text{ feet/second}$$

**Stack gas volumetric flow rate:**

$$Q_a = A_s \times V_s \times 60 = 315,193 \text{ acfm}$$

**Stack gas volumetric flow rate, wet basis:**

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] = 166,915 \text{ scfm}$$

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] \times 60 = 10,014,892 \text{ scfh}$$

**Stack gas volumetric flow rate, dry basis:**

$$Q_{std} = Q_{sw} \times (1 - B_{wo}) = 134,379 \text{ dscfm}$$

$$Q_{std} = Q_{sw} \times (1 - B_{wo}) \times 60 = 8,062,711 \text{ dscfh}$$

# USEPA Method 4 Moisture Determination Sample Calculations

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 2-A

## Data Input:

Volume metered ( $V_m$ ):	30.180 ft <sup>3</sup>
Meter calibration coefficient ( $Y_d$ ):	0.995 dimensionless
Barometric pressure ( $P_{bar}$ ):	29.29 inches Hg
Meter sample rate ( $\Delta H$ ):	0.37 inches H <sub>2</sub> O
Meter inlet/outlet temperature ( $T_m$ ):	101.6 °F
Volume of moisture collected ( $V_{lc}$ ):	142.3 milliliters
Stack Temperature ( $T_s$ ):	513.6 °F
Static Pressure ( $St$ ):	-1.0 inches H <sub>2</sub> O

## Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):

### Volume of sample, dry basis:

$$V_{m_{std}} = V_m \times Y_d \times \left( \frac{528.0^\circ R}{29.92 \text{ "Hg}} \right) \times \left( \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m + 460} \right) = 27.664 \text{ dscf}$$

### Volume of water vapor in sample:

$$V_{w_{std}} = \frac{0.04707 \text{ ft}^3}{\text{ml}} \times V_{lc} = 6.698 \text{ scf}$$

### Fractional moisture content of stack gas:

$$B_{wo} = \frac{V_{w_{std}}}{(V_{m_{std}} + V_{w_{std}})} = 0.1949 B_{wo}$$

### Percent Moisture:

$$\% \text{moisture} = B_{wo} \times 100 = 19.49 \%$$

### Fractional moisture content of stack gas at saturated conditions:

$$T_{s(K)} = ((T_s - 32) \times 0.5556) + 273 = 540.6 \text{ °Kelvin}$$

$$P_{s(\text{mmHg})} = \left( P_{bar} + \frac{S_i}{13.6} \right) \times 25.401 = 744.00 \text{ mm Hg}$$

$$B_{wos} = \frac{\sqrt{10 \left( A - \left( \frac{B}{(T_{s(K)} - C)} \right) \right)}}{P_{s(\text{mmHg})}} \quad \begin{array}{l} \text{where:} \\ A = 8.361 \\ B = 1893.5 \\ C = 27.65 \end{array} = 1.00$$

### Percent moisture at saturated conditions:

$$\% \text{moisture}_{\text{saturated}} = B_{wos} \times 100 = 100.00 \%$$

### Percent moisture used for emissions calculations:

$$= 19.49 \%$$

**USEPA Method 201A PM<sub>10</sub> Emissions  
D<sub>50</sub> Cutpoint Calculation Summary**

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 2-A

**Data Input**

Stack temperature (T <sub>s</sub> ):	513.6 °F
Fractional Moisture content (B <sub>ws</sub> ):	0.1949
Oxygen (O <sub>2</sub> ):	1.7 %
Stack pressure (P <sub>s</sub> ):	29.22 Inches Hg Abs.
Volume metered (V <sub>mstd</sub> ):	27.664 dsct
Volume of water vapor (V <sub>wstd</sub> ):	6.698 scf
Molecular weight of gas, wet basis (M <sub>s</sub> ):	28.553 lb/lb-mole
Test length (θ):	90.70 minutes
D <sub>p</sub> :	10.0 microns

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Stack gas viscosity:**

$$\mu = -150.3162 + \left(13.4622 \times \sqrt{(T_s + 460)}\right) + \left(3.86153 \times 10^{-6} \times (T_s + 460)^{-2}\right) + \left(0.591123 \times (\%O_{2, \text{wet}})\right) - \left(91.9723 \times B_{ws}\right) + \left(1.51761 \times 10^{-5} \times B_{ws} \times (T_s + 460)^2\right)$$

= 259.50 micropoise

**Sample flow rate @ standard conditions:**

$$Q_{sSt} = \frac{V_{mstd}}{\theta}$$

= 0.305 dscfm

**Sample flow rate through PM<sub>10</sub> cyclone:**

$$Q_s = \frac{29.92}{528} \times Q_{sSt} \times \left(\frac{1}{(1 - B_{ws})}\right) \times \left(\frac{(T_s + 460)}{P_s}\right)$$

= 0.715 cfm

**Calculated Reynolds Number**

$$N_{re} = 8.64 \times 10^5 \times \left(\frac{P_s \times M_s}{(T_s + 460)}\right) \times \left(\frac{Q_s}{\mu}\right)$$

= 2041

**Cunningham Correction Factor**

$$C = 1 + 0.0057193 \times \left(\frac{\mu}{P_s \times D_p}\right) \times \left(\left(\frac{(T_s + 460)}{M_s}\right)^{0.50}\right)$$

= 1.0297

**D<sub>50</sub> cutpoint (for Cyclone I):**

$$D_{50} = \left(0.15625 \times \left(\frac{(T_s + 460)}{(M_s \times P_s)}\right)^{0.2091}\right) \times \left(\frac{\mu}{Q_s}\right)^{7.091}$$

= 10.540 μm

**USEPA Method 202**  
**Condensible Particulate Calculation Summary**

COMPANY: BP  
LOCATION: Whiting, IN  
SOURCE: FCCU 500  
TEST DATE: 5/27/20  
RUN NUMBER: 2-A

**Data Input:**

$V_m$ :	30.180	ft <sup>3</sup>	$Q_s$ :	134,379	dscfm
$\gamma$ FACTOR:	0.995		$T_s$ :	513.6	°F
$P_{bar}$ :	29.29	in.Hg	Runtime:	90.70	minutes
$\Delta H$ :	0.37	in.H <sub>2</sub> O	$V_s$ :	82.575	ft/sec
$T_m$ :	101.6	°F	$P_s$ :	29.22	in.Hg
$V_c$ :	142.3	mL	Noz. diam:	0.164	inches
$N$ :	0.0000		$m_{ib}$ :	0.00	mg
$V_t$ :	0.00	mL	$m_{ob}$ :	0.00	mg
$m_r$ :	4.70	mg			
$m_o$ :	0.80	mg			

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Volume of sample at standard conditions:**

$$V_{mstd} = \left( \frac{528}{29.92} \right) \times V_m \times \gamma \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right] = 27.664 \text{ dscf}$$

**Mass of ammonia correction:**

$$m_c = 17.03 \times V_T \times N = 0.00 \text{ mg}$$

**Mass of the field blank:**

$$m_{fb} = m_{ib} + m_{ob} = 0.00 \text{ mg}$$

**Mass of inorganic condensible PM:**

$$m_i = m_r - m_c = 4.70 \text{ mg}$$

**Total mass of condensible PM:**

$$m_{cpm} = m_i + m_o - m_{fb} = 5.50 \text{ mg}$$

**USEPA Method 201A PM<sub>10</sub> Emissions  
Particulate Calculation Summary**

**Client:** BP  
**Location:** Whiting, IN  
**Source:** FCCU 500  
**Date:** 5/27/2020  
**Run #:** 2-A

**Data Input**

Barometric pressure (P <sub>bar</sub> ):	29.29 inches Hg	<b>Particulate Weight:</b>	
Stack pressure (P <sub>s</sub> ):	29.22 Inches Hg Abs.	<PM10 (Filterable)	83.80 milligrams
Test length (t):	90.70 minutes	>PM10 (Cyclone Catch)	22.30 milligrams
Sample nozzle diameter (D <sub>n</sub> ):	0.1640 inches		
Sample nozzle area (A <sub>n</sub> ):	0.000147 ft <sup>2</sup>	<PM10 (Probe Wash)	5.15 milligrams
Stack temperature (T <sub>s</sub> ):	513.6 °F	Total PM <sub>10</sub> front half:	88.95 milligrams
Volume metered (V <sub>mstd</sub> ):	27.664 ft <sup>3</sup>		
Stack gas velocity (V <sub>s</sub> ):	82.575 feet/second	Total PM front half	111.25 milligrams
Stack gas volumetric flow (Q <sub>std</sub> ):	8,062.711 dscf/hour	Total corrected PM <sub>10</sub> back half:	5.50 milligrams
Fractional moisture content (B <sub>wo</sub> ):	0.1949		
Coke Burn Rate (R <sub>c</sub> ):	35,986 lb/hr		
		Total PM <sub>10</sub> weight (M <sub>n</sub> ):	94.45 milligrams
		Total PM weight (M <sub>n</sub> ):	116.75 milligrams (>PM <sub>10</sub> + PM <sub>10</sub> )

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Percent Isokinetic:**

$$\% \text{isokinetic} = \frac{0.0945 \times V_{mstd} \times (T_s + 460)}{P_s \times V_s \times 0 \times A_n \times (1 - B_{wo})} = 98.5 \% \text{ isokinetic}$$

**PM<sub>10</sub> and Total Particulate emission rate (lb/dscf):**

$$C_s = \frac{\left( \frac{0.01543 \text{ grains}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.0651 \text{ total PM gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0124 \text{ >PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0496 \text{ filterable PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0031 \text{ condensible PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0527 \text{ PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 149.041 \text{ total PM mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 28.468 \text{ >PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 113.552 \text{ filterable PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 7.021 \text{ condensible PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 120.573 \text{ PM}_{10} \text{ mg/dscm}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 9.306 \times 10^{-6} \text{ total PM lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 1.777 \times 10^{-6} \text{ >PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 7.090 \times 10^{-6} \text{ filterable PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.438 \times 10^{-6} \text{ condensible PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 7.528 \times 10^{-6} \text{ PM}_{10} \text{ lb/dscf}$$

**PM<sub>10</sub> and Total Particulate emission rate (lb/hr):**

$$E_p = C_s \times Q_{std} = 75.030 \text{ total PM lb/hr}$$

$$E_p = C_s \times Q_{std} = 14.331 \text{ >PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 57.164 \text{ filterable PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 3.535 \text{ condensible PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 60.699 \text{ PM}_{10} \text{ lb/hr}$$

$$\text{pmr}_{\text{lb/1000lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 2.085 \text{ total PM lb/1000lb coke burn}$$

$$\text{pmr}_{\text{lb/1000lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 0.398 \text{ >PM}_{10} \text{ lb/1000lb coke burn}$$

$$\text{pmr}_{\text{lb/1000lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 1.589 \text{ filterable PM}_{10} \text{ lb/1000lb coke burn}$$

$$\text{pmr}_{\text{lb/1000lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 0.098 \text{ condensible PM}_{10} \text{ lb/1000 coke burn}$$

$$\text{pmr}_{\text{lb/1000lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 1.687 \text{ PM}_{10} \text{ lb/1000 coke burn}$$

**USEPA Method 2**  
**Volumetric Flow Rate Sample Calculations (Circular Ducts)**

Client: BP  
 Location: Whiting, IN  
 Source: FCCU 500  
 Date: 5/27/2020  
 Run #: 2-B

**Data Input**

Carbon Dioxide (CO <sub>2</sub> ):	19.0 %
Oxygen (O <sub>2</sub> ):	1.7 %
Nitrogen (N <sub>2</sub> ):	79.3 %
Fractional Moisture Content (B <sub>wo</sub> )	0.1998
Stack Temperature (T <sub>s</sub> ):	510.0 °F
Pitot Coefficient (C <sub>p</sub> ):	0.84 dimensionless
Average square root of ΔP	1.0954 inches H <sub>2</sub> O
Barometric Pressure (P <sub>bar</sub> ):	29.29 inches Hg
Static Pressure (S <sub>t</sub> ):	-0.95 inches H <sub>2</sub> O
Stack diameter:	108.00 inches H <sub>2</sub> O
Stack area (A <sub>s</sub> ):	63.6172 ft <sup>2</sup>

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Dry molecular weight of stack gas:**

$$M_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2) = 31.108 \text{ lb/lb-mole}$$

**Molecular weight of stack gas, wet basis:**

$$M_s = (M_d \times (1 - B_{ws})) + (18 \times B_{ws}) = 28.488 \text{ lb/lb-mole}$$

**Absolute stack gas pressure:**

$$P_s = P_{bar} + \left( \frac{S_t}{13.6} \right) = 29.220 \text{ inches H}_2\text{O}$$

**Stack gas velocity:**

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{(T_s + 460)}{(P_s \times M_s)}} = 84.914 \text{ feet/second}$$

**Stack gas volumetric flow rate:**

$$Q_a = A_s \times V_s \times 60 = 324,118 \text{ acfm}$$

**Stack gas volumetric flow rate, wet basis:**

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] = 172,300 \text{ scfm}$$

$$Q_{sw} = Q_a \times \left[ \left( \frac{528^\circ R}{29.92 \text{ in. Hg}} \right) \times \left( \frac{P_s}{T_s + 460} \right) \right] \times 60 = 10,337,994 \text{ scfh}$$

**Stack gas volumetric flow rate, dry basis:**

$$Q_{std} = Q_{sw} \times (1 - B_{wo}) = 137,867 \text{ dscfm}$$

$$Q_{std} = Q_{sw} \times (1 - B_{wo}) \times 60 = 8,272,031 \text{ dscfh}$$

# USEPA Method 4 Moisture Determination Sample Calculations

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 2-B

## Data Input:

Volume metered ( $V_m$ ):	32.124 ft <sup>3</sup>
Meter calibration coefficient ( $Y_d$ ):	1.009 dimensionless
Barometric pressure ( $P_{bar}$ ):	29.29 inches Hg
Meter sample rate ( $\Delta H$ ):	0.30 inches H <sub>2</sub> O
Meter inlet/outlet temperature ( $T_m$ ):	117.3 °F
Volume of moisture collected ( $V_{lc}$ ):	154.1 milliliters
Stack Temperature ( $T_s$ ):	510.0 °F
Static Pressure ( $S_t$ ):	-1.0 inches H <sub>2</sub> O

## Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):

### Volume of sample, dry basis:

$$V_{m_{std}} = V_m \times Y_d \times \left( \frac{528.0^\circ R}{29.92'' \text{ Hg}} \right) \times \left( \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m + 460} \right) = 29.043 \text{ dscf}$$

### Volume of water vapor in sample:

$$V_{w_{std}} = \frac{0.04707 \text{ ft}^3}{\text{ml}} \times V_{lc} = 7.253 \text{ scf}$$

### Fractional moisture content of stack gas:

$$B_{wo} = \frac{V_{w_{std}}}{(V_{m_{std}} + V_{w_{std}})} = 0.1998 B_{wo}$$

### Percent Moisture:

$$\% \text{moisture} = B_{wo} \times 100 = 19.98 \%$$

### Fractional moisture content of stack gas at saturated conditions:

$$T_{s(K)} = ((T_s - 32) * 0.5556) + 273 = 538.6 \text{ °Kelvin}$$

$$P_{s(\text{mmHg})} = \left( P_{bar} + \frac{S_t}{13.6} \right) \times 25.401 = 744.00 \text{ mm Hg}$$

$$B_{wos} = \frac{\sqrt[10]{\left( A \left( \frac{B}{(T_{s(K)} - C)} \right) \right)}}{P_{s(\text{mmHg})}} \quad \begin{array}{l} \text{where:} \\ A = 8.361 \\ B = 1893.5 \\ C = 27.65 \end{array} = 1.00$$

### Percent moisture at saturated conditions:

$$\% \text{moisture}_{\text{saturated}} = B_{wos} \times 100 = 100.00 \%$$

### Percent moisture used for emissions calculations:

$$= 19.98 \%$$



**USEPA Method 201A PM<sub>10</sub> Emissions  
D<sub>50</sub> Cutpoint Calculation Summary**

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 2-B

**Data Input**

Stack temperature (T <sub>s</sub> ):	510.0 °F
Fractional Moisture content (B <sub>ws</sub> ):	0.1998
Oxygen (O <sub>2</sub> ):	1.7 %
Stack pressure (P <sub>s</sub> ):	29.22 Inches Hg Abs.
Volume metered (V <sub>mstd</sub> ):	29.043 dscf
Volume of water vapor (VW <sub>sstd</sub> ):	7.253 scf
Molecular weight of gas, wet basis (M <sub>s</sub> ):	28.488 lb/lb-mole
Test length (t):	93.30 minutes
D <sub>p</sub> :	10.0 microns

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Stack gas viscosity:**

$$\mu = -150.3162 + (13.4622 \times \sqrt{(T_s + 460)}) + (3.86153 \times 10^{-5} \times (T_s + 460)^2) + (0.591123 \times (\%O_{2, \text{wet}})) - (91.9723 \times B_{ws}) + (1.51761 \times 10^{-5} \times B_{ws} \times (T_s + 460)^2)$$

= 258.3 micropoise

**Sample flow rate @ standard conditions:**

$$Q_{sSt} = \frac{V_{mstd}}{t}$$

= 0.311 dscfm

**Sample flow rate through PM<sub>10</sub> cyclone:**

$$Q_s = \frac{29.92}{528} \times Q_{sSt} \times \left( \frac{1}{(1 - B_{ws})} \right) \times \left( \frac{[T_s + 460]}{P_s} \right)$$

= 0.732 cfm

**Calculated Reynolds Number**

$$N_{re} = 8.64 \times 10^5 \times \left( \frac{P_s \times M_s}{(T_s + 460)} \right) \times \left( \frac{Q_s}{\mu} \right)$$

= 2100

**Cunningham Correction Factor**

$$C = 1 + 0.0057193 \times \left( \frac{\mu}{P_s \times D_p} \right) \times \left( \left( \frac{[T_s + 460]}{M_s} \right)^{0.50} \right)$$

= 1.030

**D<sub>50</sub> cutpoint (for Cyclone I):**

$$D_{50} = \left( 0.15625 \times \left( \frac{[T_s + 460]}{(M_s \times P_s)} \right)^{0.2091} \right) \times \left( \frac{\mu}{Q_s} \right)^{0.7091}$$

= 10.336 μm

**USEPA Method 202**  
**Condensible Particulate Calculation Summary**

COMPANY: BP  
 LOCATION: Whiting, IN  
 SOURCE: FCCU 500  
 TEST DATE: 5/27/20  
 RUN NUMBER: 2-B

**Data Input:**

V <sub>m</sub> :	32.124	ft <sup>3</sup>	Q <sub>s</sub> :	137,867	dscfm
γ FACTOR:	1.009		T <sub>s</sub> :	510.0	°F
P <sub>bar</sub> :	29.29	in.Hg	Runtime:	93.30	minutes
ΔH:	0.30	in.H <sub>2</sub> O	V <sub>s</sub> :	84.914	ft/sec
T <sub>m</sub> :	117.3	°F	P <sub>s</sub> :	29.22	in.Hg
V <sub>ic</sub> :	154.1	mL	Noz. diam:	0.164	inches
N:	0.0000		m <sub>ib</sub> :	0.00	mg
V <sub>t</sub> :	0.00	mL	m <sub>ob</sub> :	0.00	mg
m <sub>r</sub> :	5.40	mg			
m <sub>o</sub> :	0.90	mg			

**Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):**

**Volume of sample at standard conditions:**

$$V_{mstd} = \left( \frac{528}{29.92} \right) \times V_m \times \gamma \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right] = 29.043 \text{ dscf}$$

**Mass of ammonia correction:**

$$m_c = 17.03 \times V_T \times N = 0.00 \text{ mg}$$

**Mass of the field blank:**

$$m_{fb} = m_{ib} + m_{ob} = 0.00 \text{ mg}$$

**Mass of inorganic condensible PM:**

$$m_i = m_r - m_c = 5.40 \text{ mg}$$

**Total mass of condensible PM:**

$$m_{cpm} = m_i + m_o - m_{fb} = 6.30 \text{ mg}$$

# USEPA Method 201A PM10 Emissions Particulate Calculation Summary

Client: BP  
Location: Whiting, IN  
Source: FCCU 500  
Date: 5/27/2020  
Run #: 2-B

## Data Input

Barometric pressure (P <sub>bar</sub> ):	29.29 Inches Hg	Particulate Weight:	
Stack pressure (P <sub>s</sub> ):	29.22 Inches Hg Abs.	<PM10 (Filterable)	79.50 milligrams
Test length (t):	93.30 minutes	>PM10 (Cyclone Catch)	28.60 milligrams
Sample nozzle diameter (D <sub>n</sub> ):	0.1640 inches		
Sample nozzle area (A <sub>n</sub> ):	0.000147 ft <sup>2</sup>	<PM10 (Probe Wash)	4.05 milligrams
Stack temperature (T <sub>s</sub> ):	510.0 °F	Total PM <sub>10</sub> front half:	83.55 milligrams
Volume metered (V <sub>mstd</sub> ):	29.043 ft <sup>3</sup>		
Stack gas velocity (V <sub>s</sub> ):	84.914 feet/second	Total PM front half	112.15 milligrams
Stack gas volumetric flow (Q <sub>std</sub> ):	8,272.031 dscf/hour	Total corrected PM <sub>10</sub> back half:	6.30 milligrams
Fractional Moisture content (B <sub>wo</sub> ):	0.1998		
Coke Burn Rate (R <sub>c</sub> ):	35,986 lb/hr	Total PM <sub>10</sub> weight (M <sub>n</sub> ):	89.85 milligrams
		Total PM weight (M <sub>n</sub> ):	118.45 milligrams (>PM <sub>10</sub> + PM <sub>10</sub> )

## Sample calculations @ standard conditions (29.92 inches Hg, 68.0 °F):

### Percent Isokinetic:

$$\% \text{isokinetic} = \frac{0.0945 \times V_{mstd} \times (T_s + 460)}{P_s \times V_s \times t \times A_n \times (1 - B_{wo})} = 98.0 \% \text{ isokinetic}$$

### PM<sub>10</sub> and Total Particulate emission rate (lb/dscf):

$$C_s = \frac{\left( \frac{0.01543 \text{ grains}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.0629 \text{ total PM gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0162 \text{ >PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0444 \text{ filterable PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0033 \text{ condensible PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 0.0477 \text{ PM}_{10} \text{ gr/dscf}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 144.032 \text{ total PM mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 34.777 \text{ >PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 101.594 \text{ filterable PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 7.661 \text{ condensible PM}_{10} \text{ mg/dscm}$$

$$C_s = \frac{M_n}{V_{mstd}} \times \frac{35.315 \text{ ft}^3}{\text{m}^3} = 109.256 \text{ PM}_{10} \text{ mg/dscm}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 8.993 \times 10^{-6} \text{ total PM lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 2.171 \times 10^{-6} \text{ >PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 6.343 \times 10^{-6} \text{ filterable PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 0.478 \times 10^{-6} \text{ condensible PM}_{10} \text{ lb/dscf}$$

$$E_p = \frac{\left( \frac{2.205 \times 10^{-6} \text{ lb}}{\text{mg}} \times M_n \right)}{V_{mstd}} = 6.822 \times 10^{-6} \text{ PM}_{10} \text{ lb/dscf}$$

### PM<sub>10</sub> and Total Particulate emission rate (lb/hr):

$$E_p = C_s \times Q_{std} = 74.391 \text{ total PM lb/hr}$$

$$E_p = C_s \times Q_{std} = 17.962 \text{ >PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 52.472 \text{ filterable PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 3.957 \text{ condensible PM}_{10} \text{ lb/hr}$$

$$E_p = C_s \times Q_{std} = 56.429 \text{ PM}_{10} \text{ lb/hr}$$

$$p_{\text{PM}_{10} \text{ lb}/1000 \text{ lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 2.067 \text{ total PM lb/1000lb coke burn}$$

$$p_{\text{PM}_{10} \text{ lb}/1000 \text{ lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 0.499 \text{ >PM}_{10} \text{ lb/1000lb coke burn}$$

$$p_{\text{PM}_{10} \text{ lb}/1000 \text{ lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 1.458 \text{ filterable PM}_{10} \text{ lb/1000lb coke burn}$$

$$p_{\text{PM}_{10} \text{ lb}/1000 \text{ lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 0.110 \text{ condensible PM}_{10} \text{ lb/1000 coke burn}$$

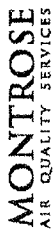
$$p_{\text{PM}_{10} \text{ lb}/1000 \text{ lb coke burn}} = \frac{(E_p)(1000)}{(R_c)} = 1.568 \text{ PM}_{10} \text{ lb/1000 coke burn}$$

## **ATTACHMENT B FIELD DATA**

Project Information				Sampling Conditions				Equipment Checks				Intermediate Leak Check Volume, ft <sup>3</sup>				Office Pressure				Velocity Head				DGM Reading				Clock Time				Sensitivity			
Date <u>5/27/20</u> Project # <u>024AS-748176</u>				Static Pressure, in. H <sub>2</sub> O <u>-1.0</u> Ambient Temp, °F <u>90</u>				Pilot (+), pass @ in. H <sub>2</sub> O <u>4.6</u> Mid <u>5.1</u> Post <u>5.1</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>549.445</u>				Clock Time 24hr <u>0800</u>				Sensitivity <u>0.0-0.001</u>							
Customer/Facility <u>BP WHITING</u>				Barometric Pressure, in. Hg <u>29.24</u> Ref. Barometer ID <u>7-8</u>				Pilot (-), pass @ in. H <sub>2</sub> O <u>5.3</u> Mid <u>5.3</u> Post <u>5.3</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>563.260</u>				Clock Time 24hr <u>0900</u>				Sensitivity <u>0.0-0.001</u>							
Unit ID/Sample Location <u>FCCU 500</u>				Wind Speed / Direction <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>559.98</u>				Clock Time 24hr <u>0910</u>				Sensitivity <u>0.0-0.001</u>							
Run # <u>1A</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>563.25</u>				Clock Time 24hr <u>0930</u>				Sensitivity <u>0.0-0.001</u>							
Sampling Equipment IDs				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>566.57</u>				Clock Time 24hr <u>0940</u>				Sensitivity <u>0.0-0.001</u>							
Meterbox ID <u>611209</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>569.74</u>				Clock Time 24hr <u>0950</u>				Sensitivity <u>0.0-0.001</u>							
Umbilical ID <u>32</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>570.96</u>				Clock Time 24hr <u>1000</u>				Sensitivity <u>0.0-0.001</u>							
Nozzle ID <u>3</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>576.92</u>				Clock Time 24hr <u>1010</u>				Sensitivity <u>0.0-0.001</u>							
Pilot / Probe ID <u>567</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>579.61</u>				Clock Time 24hr <u>1020</u>				Sensitivity <u>0.0-0.001</u>							
Manometer ID <u>611209</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>582.85</u>				Clock Time 24hr <u>1030</u>				Sensitivity <u>0.0-0.001</u>							
Sensitivity <u>0.0-0.001</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>586.11</u>				Clock Time 24hr <u>1040</u>				Sensitivity <u>0.0-0.001</u>							
K-Factor <u>4.47</u>				Probe / Filter Temp Range, °F <u>24</u>				Pilot visual inspection <u>pass</u>				Target <u>.35</u> Actual <u>.35</u>				Target <u>.35</u> Actual <u>.35</u>				DGM Reading, Vm, ft <sup>3</sup> <u>589.350</u>				Clock Time 24hr <u>1050</u>				Sensitivity <u>0.0-0.001</u>							
A 1	0	0800	549.445	1.1	.35	.35	510	257	256	225	63	98	91	69	3																				
1	19:52	0910	563.260	1.1	.35	.35	511	257	258	236	58	101	92	68	3																				
1	30:14	0920	559.98	1.1	.35	.35	510	256	254	230	58	104	91	69	3																				
1	40:19	0930	563.25	1.1	.35	.35	512	261	259	232	60	104	92	71	3																				
1	50:06	0940	566.57	1.1	.35	.35	510	258	256	235	60	107	91	73	3																				
1	60:02	0950	569.74	1.1	.35	.35	512	255	257	236	61	111	93	74	3																				
1	69:58	1000	570.96	1.2	.35	.35	510	256	255	230	63	113	93	76	3																				
1	80:10	1010	576.92	1.2	.35	.35	511	255	256	238	65	114	94	78	3																				
1	90:32	1020	579.61	1.1	.35	.35	512	260	255	236	65	119	95	78	3																				
1	100:28	1030	582.85	1.1	.35	.35	510	248	250	235	62	115	97	73	3																				
1	110:24	1040	586.11	1.1	.35	.35	512	247	251	238	63	114	97	74	3																				
1	120:20	1050	589.350																																
Averages																																			



001AS-QMS-FM-225

[illegible]



**Project Information**

 Date 5/27/20 Project # 024AS-748176  
 Customer / Facility BP WHITE NB  
 Unit ID / Sample Location FCCU 500  
 Run # 1A-2A / 10-2B Operator MC/JC/SF
**Equipment Identification**

 Ref. Thermometer \_\_\_\_\_  
 Hygrometer \_\_\_\_\_  
 Field Balance T-8  
 Check Weights T-8  
 Calipers M13
**Balance Audit** (Field balance must be within 0.5g of check weight mass)

 Date 5/27/20  
 Standard mass, g 500.0  
 Field balance mass, g 499.1
**Ambient Conditions** (Mobile Lab)

 Relative humidity, % \_\_\_\_\_  
 Temperature, °F 80  
 Mobile lab # T-8
**Moisture Determination**

	Run 1			Run 2			Run 3			
Contents	Initial	Final	Net	Initial	Final	Net	Initial	Final	Net	
Knockout	N/A	394.2	571.5	177.3	392.8	561.3	168.5	379.3	508.5	142.179
Impinger 1	N/A	676.8	678.6	1.8	673.2	693.2	20.0	667.9	669.7	1.8
Impinger 2	H <sub>2</sub> O	739.4	742.4	2.5	756.0	761.0	4.8	720.1	722.4	2.3
Impinger 3	S-G	809.8	823.3	13.5	886.4	904.8	18.4	842.3	851.3	9.0
Impinger 4										
Impinger 5										
Impinger 6										
Impinger 7										
Impinger 8										
Silica Gel										
Line Rinse										
Train Net Gain (Vlc)			195.1			211.7				142.3

**Nozzle Measurements** (Difference between any two measurements must not be more than 0.004 in (0.1 mm))

 Nozzle 1 diameters 0.164 D1 0.164 D2 0.164 D3 0.164 Average A  
 Nozzle 2 diameters 0.164 D1 0.164 D2 0.164 D3 0.164 Average B  
 Nozzle 3 diameters \_\_\_\_\_ D1 \_\_\_\_\_ D2 \_\_\_\_\_ D3 \_\_\_\_\_ Average \_\_\_\_\_

 Nozzle Material ☐ quartz ☐ glass ☒ steel ☐ titanium ☐ inconel ☐ other \_\_\_\_\_

 Probe Type ☒ heated ☐ unheated ☐ air-cooled ☐ water-cooled ☐ other \_\_\_\_\_

 Probe Liner ☐ quartz ☐ glass ☒ steel ☐ Teflon ☐ other \_\_\_\_\_

**Filter Information**

 Front Half: ☒ quartz fiber ☐ glass fiber ☐ Teflon ☐ Teflon/quartz ☐ other \_\_\_\_\_

Filter Number: Run 1: \_\_\_\_\_ Run 2: \_\_\_\_\_ Run 3: \_\_\_\_\_ Run \_\_\_\_\_

 Back Half: ☐ quartz fiber ☐ glass fiber ☐ Teflon ☐ Teflon/quartz ☐ other \_\_\_\_\_

**Reagent Information**

 Type Lot Number  
ACETONE 0000242182  
DI 0000237576  
HEXANE 173874
**Sample Observations**
7 MTK 5/29

 QA/QC Check: Completeness ☒ Legibility ☒ Accuracy ☒ Specifications ☒

 Checked by: M. KRUEGER Team Leader: \_\_\_\_\_

<b>Project Information</b>		<b>Equipment Identification</b>
Date <u>5/27/20</u>	Project # <u>OLYAS-748176</u>	Ref. Thermometer _____
Customer / Facility <u>BP Whiting</u>		Hygrometer _____
Unit ID / Sample Location <u>FCCU 500</u>		Field Balance <u>T-8</u>
Run # <u>2B</u>	Operator <u>MK/JC/SP</u>	Check Weights <u>T-8</u>
		Calipers <u>M/B</u>

<b>Balance Audit</b> (Field balance must be within 0.5g of check weight mass)		<b>Ambient Conditions (Mobile Lab)</b>
Date <u>5/27</u>		Relative humidity, % _____
Standard mass, g <u>500.0</u>		Temperature, °F _____
Field balance mass, g <u>499.9</u>		Mobile lab # <u>T-8</u>

<b>Moisture Determination</b>									
	Run 1			Run 2			Run 3		
Contents	Initial	Final	Net	Initial	Final	Net	Initial	Final	Net
Knockout <u>KO</u>	<u>371.8</u>	<u>508.9</u>	<u>137.1</u>						
Impinger 1 <u>MT</u>	<u>806.3</u>	<u>809.0</u>	<u>2.7</u>						
Impinger 2 <u>DE</u>	<u>684.0</u>	<u>685.1</u>	<u>1.1</u>						
Impinger 3 <u>SG</u>	<u>220.0</u>	<u>213.2</u>	<u>13.2</u>						
Impinger 4									
Impinger 5									
Impinger 6									
Impinger 7									
Impinger 8									
Silica Gel									
Line Rinse									
Train Net Gain (Vlc)	<u>154.1</u>								

<b>Nozzle Measurements</b> (Difference between any two measurements must not be more than 0.004 in (0.1 mm))						
Nozzle 1 diameters	D1	D2	D3	Average		
Nozzle 2 diameters	D1	D2	D3	Average		
Nozzle 3 diameters	D1	D2	D3	Average		
<b>Nozzle Material</b>	<input type="checkbox"/> quartz	<input type="checkbox"/> glass	<input type="checkbox"/> steel	<input type="checkbox"/> titanium	<input type="checkbox"/> inconel	<input type="checkbox"/> other _____
<b>Probe Type</b>	<input type="checkbox"/> heated	<input type="checkbox"/> unheated	<input type="checkbox"/> air-cooled	<input type="checkbox"/> water-cooled	<input type="checkbox"/> other _____	
<b>Probe Liner</b>	<input type="checkbox"/> quartz	<input type="checkbox"/> glass	<input type="checkbox"/> steel	<input type="checkbox"/> Teflon	<input type="checkbox"/> other _____	

<b>Filter Information</b>	
Front Half:	<input type="checkbox"/> quartz fiber <input type="checkbox"/> glass fiber <input type="checkbox"/> Teflon <input type="checkbox"/> Teflon/quartz <input type="checkbox"/> other _____
Filter Number:	Run 1: _____ Run 2: _____ Run 3: _____ Run _____:
Back Half:	<input type="checkbox"/> quartz fiber <input type="checkbox"/> glass fiber <input type="checkbox"/> Teflon <input type="checkbox"/> Teflon/quartz <input type="checkbox"/> other _____

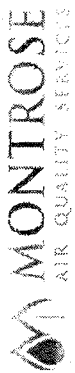
<b>Reagent Information</b>	<b>Sample Observations</b>
Type _____ Lot Number _____	

 QA/QC Check: Completeness ☒ Legibility ☒ Accuracy ☒ Specifications ☒

 Checked by: M. KRUEBER Team Leader: \_\_\_\_\_

001AS-QMS-FM-226

## **ATTACHMENT C LABORATORY DATA**



## ANALYTICAL SUMMARY

CLIENT: BP

LOCATION: Whiting, IN

SOURCE: FCU 500

SAMPLE DATE: 5/27/2020

ANALYSIS: Particulates

METHOD: USEPA Method 201/202

page 1 of 2

Analyst: J. Ruggaber

Date of Completion: 6/5/2020

Template Control ID: USEPA-M201/202-PARTIC-TEMPLATE-62T-REV3

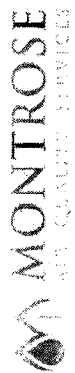
Project Number: 08-1414

### Method 201A Filterable PM

Identification	LIMS Number	Solvent Mass (g)	Tare	WT1	WT2	WT 1 - WT 2 (mg)	% difference	Particulate (mg)	Blank Corrected Particulate (mg)
Run 1A Filter	30320	-	825.2	938.7	938.8	-0.10	N/A	113.55	-
Run 1A >PM10	30315	31.1	3584.4	3619.2	3619.1	0.10	N/A	34.75	34.75
Run 1A ≤ 10PM	30316	168.1	3620.0	3633.8	3633.5	0.30	N/A	13.65	13.65
Run 1B Filter	30326	-	824.7	943.2	943.2	0.00	N/A	118.50	-
Run 1B >PM10	30321	36.4	3731.5	3767.9	3768.0	-0.10	N/A	36.45	36.45
Run 1B ≤ 10PM	30322	96.6	3946.3	3957.3	3957.5	-0.20	N/A	11.10	11.10
Run 2A Filter	30333	-	823.7	907.4	907.6	-0.20	N/A	83.80	-
Run 2A >PM10	30328	28.8	3956.3	3978.6	3978.6	0.00	N/A	22.30	22.30
Run 2A ≤ 10PM	30329	103.1	3929.1	3934.4	3934.1	0.30	N/A	5.15	5.15
Run 2B Filter	30339	-	835.8	915.3	915.3	0.00	N/A	79.50	-
Run 2B >PM10	30334	31.7	3847.3	3875.8	3876.0	-0.20	N/A	28.60	28.60
Run 2B ≤ 10PM	30335	83.8	3874.9	3878.9	3879.0	-0.10	N/A	4.05	4.05
Acetone Blank	30340	78.1	3793.8	3793.7	3793.7	0.00	N/A	<0.10	-

### M202 Organic Fraction

Identification	LIMS Number	Tare	WT1	WT2	WT 1 - WT 2 (mg)	% difference	Organic CPM (mg)
Run 1A	30318	3910.6	3912.2	3912.2	0.00	N/A	1.60
Run 1B	30324	3791.3	3792.8	3792.8	0.00	N/A	1.50
Run 2A	30331	3928.0	3928.7	3928.9	-0.20	N/A	0.80
Run 2B	30337	3778.4	3779.2	3779.4	-0.20	N/A	0.90
Acetone Blank	30341	3547.6	3547.5	3547.6	-0.10	N/A	<0.10
Hexane Blank	30327	3611.3	3611.3	3611.2	0.10	N/A	<0.10



## ANALYTICAL SUMMARY

CLIENT: BP

LOCATION: Whiting, IN

SOURCE: FCU 500

SAMPLE DATE: 5/27/2020

ANALYSIS: Particulates

METHOD: USEPA Method 201/202

page 2 of 2

Analyst: J. Ruggaber

Date of Completion: 6/5/2020

Template Control ID: USEPA-M201/202-PARTIC-TEMPLATE-62T-REV3

Project Number: 08-1414

### M202 Aqueous Fraction

Identification	LIMS Number	Tare	WT1	WT2	WT 1 - WT 2 (mg)	% difference	Inorganic CPM (mg)
Run 1A	30317	3489.9	3496.6	3496.8	-0.20	N/A	6.80
Run 1B	30323	3804.9	3814.1	3814.4	-0.30	N/A	9.35
Run 2A	30330	3919.0	3923.6	3923.8	-0.20	N/A	4.70
Run 2B	30336	3820.3	3825.6	3825.8	-0.20	N/A	5.40
DI Water Blank	30342	3562.9	3563.1	3563.1	0.00	N/A	0.20



951 Old Rand Road # 106  
Wauconda, IL 60084

### Montrose Air Quality Services Analytical Report

BP-Whiting  
Whiting, IN  
FCU-500

Lab Project #: 08-1414  
Project Manager: Steve Flaherty  
Received: 5/29/2020  
Reported: 6/5/2020

Sample ID: 1-A >PM10  
Lab Sample #: 30315

Date Sampled: 05/27/2020  
Field #: 32062

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	34.75	mg	

Sample ID: 1-A PW  
Lab Sample #: 30316

Date Sampled: 05/27/2020  
Field #: 32063

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	13.65	mg	

Sample ID: 1-A Imps  
Lab Sample #: 30317

Date Sampled: 05/27/2020  
Field #: 32064

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Inorganic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	6.80	mg	

Sample ID: 1-A Organics  
Lab Sample #: 30318

Date Sampled: 05/27/2020  
Field #: 32065

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Organic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	1.60	mg	

Sample ID: 1-A CPM Filter  
Lab Sample #: 30319

Date Sampled: 05/27/2020  
Field #: 32066

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
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Sample ID: 1-A Filter  
Lab Sample #: 30320

Date Sampled: 05/27/2020  
Field #: 31769

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
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951 Old Rand Road # 106  
Wauconda, IL 60084

### Montrose Air Quality Services Analytical Report

BP-Whiting  
Whiting, IN  
FCU-500

Lab Project #: 08-1414  
Project Manager: Steve Flaherty  
Received: 5/29/2020  
Reported: 6/5/2020

Particulate Method 201A Joel Ruggaber 06/05/2020 113.55 mg

Sample ID: 1-B >PM10  
Lab Sample #: 30321

Date Sampled: 05/27/2020  
Field #: 32067

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	36.45	mg	

Sample ID: 1-B PW  
Lab Sample #: 30322

Date Sampled: 05/27/2020  
Field #: 32083

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	11.10	mg	

Sample ID: 1-B Imps  
Lab Sample #: 30323

Date Sampled: 05/27/2020  
Field #: 32089

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Inorganic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	9.35	mg	

Sample ID: 1-B Organics  
Lab Sample #: 30324

Date Sampled: 05/27/2020  
Field #: 32070

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Organic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	1.50	mg	

Sample ID: 1-B CPM Filter  
Lab Sample #: 30325

Date Sampled: 05/27/2020  
Field #: 32081

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
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Sample ID: 1-B Filter  
Lab Sample #: 30326

Date Sampled: 05/27/2020  
Field #: 28175

Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
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Wauconda, IL 60084

### Montrose Air Quality Services Analytical Report

BP-Whiting Whiting, IN FCU-500				Lab Project #:	08-1414	
				Project Manager:	Steve Flaherty	
				Received:	5/29/2020	
				Reported:	6/5/2020	
Particulate	Method 201A	Joel Ruggaber	06/05/2020	118.50	mg	
Sample ID:	Hexane Blank			Date Sampled:	05/27/2020	
Lab Sample #:	30327			Field #:	32087	
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Organic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	<0.10	mg	
Sample ID:	2-A >PM10			Date Sampled:	05/27/2020	
Lab Sample #:	30328			Field #:	32082	
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	22.30	mg	
Sample ID:	2-A PW			Date Sampled:	05/27/2020	
Lab Sample #:	30329			Field #:	32083	
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	5.15	mg	
Sample ID:	2-A Imps			Date Sampled:	05/27/2020	
Lab Sample #:	30330			Field #:	32061	
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Inorganic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	4.70	mg	
Sample ID:	2-A Organics			Date Sampled:	05/27/2020	
Lab Sample #:	30331			Field #:	32084	
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Organic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	0.80	mg	
Sample ID:	2-A CPM Filter			Date Sampled:	05/27/2020	
Lab Sample #:	30332			Field #:	32071	
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes





951 Old Rand Road # 106  
Wauconda, IL 60084

### Montrose Air Quality Services Analytical Report

BP-Whiting  
Whiting, IN  
FCU-500

Lab Project #: 08-1414  
Project Manager: Steve Flaherty  
Received: 5/29/2020  
Reported: 6/5/2020

Sample ID:	2-A Filter	Date Sampled:	05/27/2020			
Lab Sample #:	30333	Field #:	28174			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	83.80	mg	

Sample ID:	2-B >PM10	Date Sampled:	05/27/2020			
Lab Sample #:	30334	Field #:	32072			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	28.60	mg	

Sample ID:	2-B PW	Date Sampled:	05/27/2020			
Lab Sample #:	30335	Field #:	32073			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	4.05	mg	

Sample ID:	2-B Imps	Date Sampled:	05/27/2020			
Lab Sample #:	30336	Field #:	32074			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Inorganic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	5.40	mg	

Sample ID:	2-B Organics	Date Sampled:	05/27/2020			
Lab Sample #:	30337	Field #:	32075			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Organic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	0.90	mg	

Sample ID:	2-B CPM Filter	Date Sampled:	05/27/2020			
Lab Sample #:	30338	Field #:	32076			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes



951 Old Rand Road # 106  
Wauconda, IL 60084

### Montrose Air Quality Services Analytical Report

BP-Whiting  
Whiting, IN  
FCU-500

Lab Project #: 08-1414  
Project Manager: Steve Flaherty  
Received: 5/29/2020  
Reported: 6/5/2020

Sample ID:	2-B Filter	Date Sampled:	05/27/2020			
Lab Sample #:	30339	Field #:	28183			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	79.50	mg	

Sample ID:	201A Acetone Blank	Date Sampled:	05/27/2020			
Lab Sample #:	30340	Field #:	32086			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Particulate	Method 201A	Joel Ruggaber	06/05/2020	<0.10	mg	

Sample ID:	202 Acetone Blank	Date Sampled:	05/27/2020			
Lab Sample #:	30341	Field #:	32088			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Organic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	<0.10	mg	

Sample ID:	DI Water Blank	Date Sampled:	05/27/2020			
Lab Sample #:	30342	Field #:	32085			
Analyte	Method	Analyst	Analysis Date	Result	Units	Notes
Inorganic Residue	USEPA Method 202	Joel Ruggaber	06/05/2020	0.20	mg	

Notes:

NA - Sample not tested for this analyte.

D - Value calculated from dilution.

J - Value less than the low standard but above the Limit of Detection (LOD).

L - Sample leaked before receipt.

H - Value greater than the high standard.

X - Quality control deficiency or failure observed.\

NR - Value not reported per project manager request

## Sample Receipt Checklist

Client Name: BP

Site Location: Whiting, IN

Montrose Project Manager: Steve Flaherty

Sample Collection Date(s): 5/27/20

Chain-of-Custody Number(s): 02936, 02934

Chain-of-Custody Form(s):

Custody release signatures, dates, and times present:	Yes
Preservation code noted:	Yes
Project information clearly identified:	Yes
Sample information clearly identified:	Yes
Analysis request clearly identified:	Yes
Report tier level noted:	Yes

### Sample Containers:

Quantity of samples match number on the COC	Yes
Container label ID numbers and descriptions match COC	Yes
All containers received in good condition	Yes
Liquid levels at marked heights on containers	Yes
All container labels are legible	Yes
All sample IDs are unique	Yes
Samples received in correct container type	Yes
Samples received within the required holding time	Yes
Samples received under the required preservation code	Yes
Sample receipt temperature (°F) <input type="text"/> Meets applicable method limit	N/A

### Non-Conformances and/or Corrective Actions Applied:

All of the criteria for sample acceptance have been met.

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Samples Received by: Joel Ruggaber

  
signature

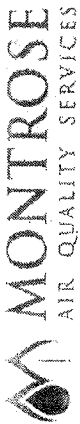
Date and Time received: 5/29/20 11:00



Chain of Custody Record Number: 02036

M024-AS-748176-RT-589

Lab Project No. (Lab use only) 02-1414		Client Name BP	Client Location Whiting, IN	MAQS Project Number 446-748176		MAQS Test Plan Number NA - Engineering	MAQS Project Manager STEVE FEATHERY					
MAQS Sampler Name F/104/06/UK		Laboratory (Wauconda or Pasadena) Wauconda		Subcontracted Laboratory (if applicable) NA		Preservation Code 1 = Ambient Temp. 2 = 4°C (Ice Packs) 3 = Dry Ice 4 = Other (Noted)						
Engineering or Compliance Test Samples		Number of Containers		Container Type (Petri, Bottle, Bag, Tube, Summa, Bomb)		Analysis Request <sup>1</sup>		Preservation Code				
Label Number	Sample Date	Time of Collection <sup>2</sup>	Sample Identification		Number of Containers		Container Type		Analysis Request <sup>1</sup>		Preservation Code	
32062	5-27		1-A > PM10		1	200			X	USEPA Method	1 = Ambient Temp.	
32063			1-A PM		1	200			X	USEPA Method	2 = 4°C (Ice Packs)	
32064			1-A Temp		1	200			X	USEPA Method	3 = Dry Ice	
32065			1-A Organics		1	200			X	USEPA Method	4 = Other (Noted)	
32066			1-A CPM		1	200			X	USEPA Method		
32067	3/27/9		1-A Filter		1	200			X	USEPA Method		
32068			1-B > PM10		1	200			X	USEPA Method		
32069			1-B PM		1	200			X	USEPA Method		
32070			1-B Temp		1	200			X	USEPA Method		
32071			1-B Organics		1	200			X	USEPA Method		
32072			1-B CPM		1	200			X	USEPA Method		
32073			1-B Filter		1	200			X	USEPA Method		
32074			Headspace Blank		1	200			X	USEPA Method		
Special Instructions:												
(1) Relinquished By				(2) Relinquished By				(3) Relinquished By				
(1) Date / Time 5/27/00 @ 1630				(2) Date / Time 5/28/00 @ 1200				(3) Date / Time				
(1) Company Montrose				(2) Company Montrose				(3) Company				
(1) Received By Van Kuy				(2) Received By				(3) Received By				
(1) Date / Time 5/28/00 2:00 PM				(2) Date / Time 5/29/00 1100				(3) Date / Time				
(1) Company Montrose				(2) Company Montrose				(3) Company				
Date test results needed: 6-12-00				Reporting level: Engineering				SHIPMENT: Hand-Carry FedEx UPS				
Route results through: FEATHERY				Project manager signature: Steve Feathery				Custody Seal Applied Yes No				



Chain of Custody Record Number: 02034

M024AS-748176-RT-589

Lab Project No. (Lab use only) 08-1414	Client Name BP	Client Location Whiting, TN	Number of Containers	Container Type (Petri, Bottle, Bag, Tube, Summa, Bomb)	Preservation Code	Analysis Request <sup>1</sup>	Preservation Code
MAQS Project Number 08-1414	MAQS Test Plan Number	MAQS Project Manager Patterson					
MAQS Sampler Name 08-1414	Laboratory (Wauconda or Pasadena) Wauconda	Subcontracted Laboratory (if applicable) Wauconda					
Engineering or Compliance Test Samples Engineering							
Label Number	Sample Date	Time of Collection <sup>2</sup>	Sample Identification				
32072	5-27		2-A 7PM10	250W			
32083			2-A 7PM	250W			
32061			2-A 7PM	250W			
32084			2-A 7PM	250W			
32071			2-A 7PM	250W			
32072			2-A 7PM	250W			
32073			2-A 7PM	250W			
32074			2-A 7PM	250W			
32075			2-A 7PM	250W			
32076			2-A 7PM	250W			
32083			2-A 7PM	250W			
32086			2-A 7PM	250W			
32088			2-A 7PM	250W			
32085			2-A 7PM	250W			
Special Instructions:				(1) Relinquished By	(2) Relinquished By	(3) Relinquished By	SHIPMENT:
				(1) Date / Time 5/27/10 @ 1630	(2) Date / Time 5/28/10 1200	(3) Date / Time	Hand Carry
				(1) Company MONTROSE	(2) Company MONTROSE	(3) Company	FedEx
Date test results needed:				(1) Received By	(2) Received By	(3) Received By	UPS
Reporting level: Engineering				(1) Date / Time 5/27/10 @ 1700	(2) Date / Time 5/28/10 1100	(3) Date / Time	Custody Seal
Route results through: Patterson				(1) Company MONTROSE	(2) Company MONTROSE	(3) Company	Applied
Project manager signature:				(1) Date / Time 5/27/10 @ 1700	(2) Date / Time 5/28/10 1100	(3) Date / Time	Yes
				(1) Company MONTROSE	(2) Company MONTROSE	(3) Company	No

## **THIS IS THE LAST PAGE OF THIS DOCUMENT**

If you have any questions, please contact one of the following individuals by email or phone.

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